

## SYNERGIC EFFECT BETWEEN INORGANIC SALTS AND $\gamma$ -Al<sub>2</sub>O<sub>3</sub> FOR XYLOSE DEHYDRATION TO FURFURAL

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### Introduction

Lignocellulosic biomass, with a high content of hemicellulose, is the main source of pentoses, from which biofuels and value-added chemicals can be produced. Amongst the latter, 2-Furfuraldehyde (furfural, FUR) is the only unsaturated organic compound prepared from carbohydrates, obtained by acid-catalyzed dehydration of xylose (XYL) [1]. Different acid solid catalysts have been studied as alternative to conventional mineral acids, which are employed in industry. Moreover, the addition of inorganic salts to improve furfural yield, especially in biphasic systems, has been previously reported in the literature [2]. In this work, the dehydration of XYL in a biphasic water:toluene system with a mesoporous  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> has been studied, and the effect of the presence of CaCl<sub>2</sub> or MgCl<sub>2</sub> in the reaction medium on the catalytic performance was evaluated.

### Experimental

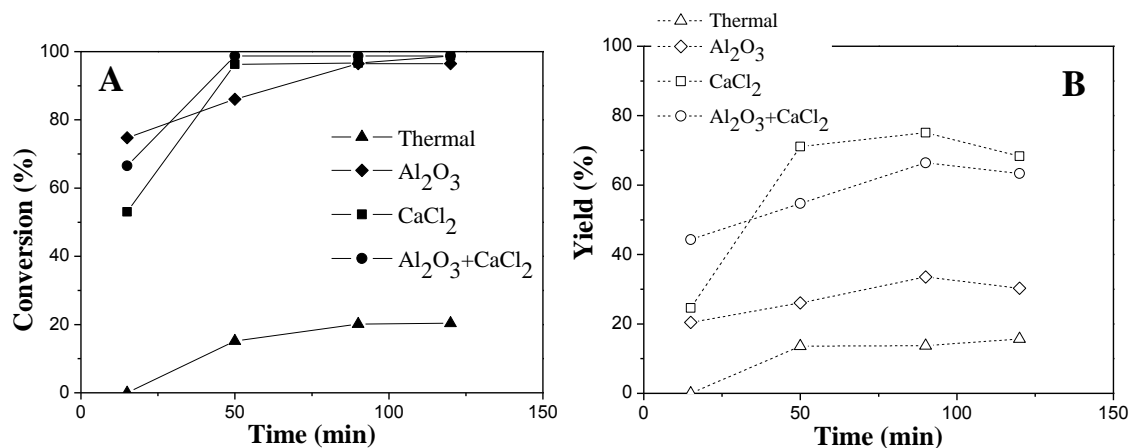
The catalytic dehydration was carried out under batch operations, by using a water:toluene biphasic system, in a glass reactor (Ace, 15 mL), with a thermostated bath and magnetic stirring, in the presence of  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> (Alfa-Aesar, 158 m<sup>2</sup>·g<sup>-1</sup> y 478  $\mu$ mol NH<sub>3</sub>·g<sup>-1</sup>) as catalyst. The experiments were carried out by mixing 50 mg of catalyst and 150 mg xylose in 1.5 ml of deionized water and 3.5 ml of toluene. The reaction products were analyzed by HPLC. Some preliminary results concerning the use of sugar liquors derived from the treatment of lignocellulosic biomass, as feedstock instead of commercial xylose, have been obtained.

### Results and discussions.

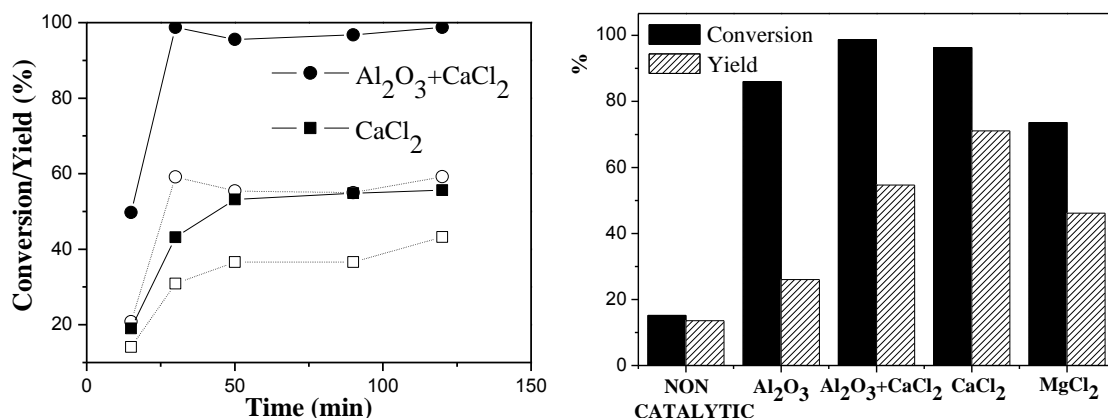
The presence of CaCl<sub>2</sub> and the use of  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> in the reaction medium for xylose dehydration to furfural were studied and compared to the non-catalytic process, at 175 °C (Fig. 1A). In all cases, high conversion values were attained with respect to the non-catalytic process.  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> shows a high activity, with a XYL conversion of 96%, after 90 min of reaction, but the furfural yield was lower than expected due to alumina favored secondary reactions [3] (Fig. 1B). It has been previously demonstrated that alkaline earth cations, like Ca<sup>2+</sup> interact with glucose molecules, accelerating considerably their dehydration, so it would be possible that they also exert a similar effect on the dehydration of xylose [4]. Thus, high furfural yields were achieved by using CaCl<sub>2</sub> even in absence of catalyst under these experimental conditions. However,

considering that side reactions are favored at high temperatures, the catalytic process was studied with  $\text{CaCl}_2$  and  $\gamma\text{-Al}_2\text{O}_3$  at  $150^\circ\text{C}$  (Fig. 2). At this lower temperature, a synergistic effect can be inferred between  $\gamma\text{-Al}_2\text{O}_3$  and  $\text{CaCl}_2$ , reaching values of XYL conversion and FUR yield of 99% and 59%, respectively, after only 30 min of reaction.

Moreover, the effect of the addition of  $\text{CaCl}_2$  and  $\text{MgCl}_2$  was compared (Fig. 3), adding the same number of moles, corresponding to 0.65 and 0.39  $\text{g}_{\text{salt}} \cdot \text{g}_{\text{aq.sol.}}$ , respectively. Although both salts improved the catalytic performance,  $\text{CaCl}_2$  is more beneficial than  $\text{MgCl}_2$ . The reaction mechanism has been studied by  $^1\text{H}$  NMR.



**Figure 1.** Xylose conversion (A) and furfural yield (B) as a function of reaction time in presence of  $\gamma\text{-Al}_2\text{O}_3$  and/or  $\text{CaCl}_2$  ( $175^\circ\text{C}$  and xylose:catalyst weight ratio = 3: 1).



**Figure 2.** Evolution of XYL conversion (■, ●) and FUR yield (□, ○) with the time ( $150^\circ\text{C}$ , xylose:catalyst weight ratio= 3:1).

**Figure 3.** Influence of the addition of  $\text{CaCl}_2$  and  $\text{MgCl}_2$  to the reaction medium ( $175^\circ\text{C}$ , 50 min and xylose:catalyst weight ratio= 3:1).

### Acknowledgements

The authors are grateful to financial support from the Spanish Ministry of Economy and Competitiveness (CTQ2015-64226-C3-3-R project).

### References

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